

1 Hemodynamics

1.1 Casson fluid – flow rate

Blood flows in a tube of radius 1 cm because of a pressure gradient of 0.4 dynes/cm^3 . Treating the blood as a Casson fluid with yield stress 0.06 dynes/cm^2 , what percentage of the total volume flowrate is from blood traveling in the central non-flowing "core" of the flow?

$$\frac{dp}{dx} = 0.4 \frac{\text{dyn}}{\text{cm}^3}$$

$$\tau_y = 0.06 \frac{\text{dyn}}{\text{cm}^2}$$



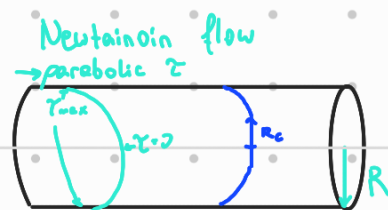
$$\tau(R_c) = \tau_y = \frac{R_c}{2} \cdot \frac{dp}{dx} \Rightarrow R_c = 0.3 \text{ cm}$$

Steady flow: $\tau(r) = \frac{r}{2} \frac{dp}{dx}$

Casson relationship: $\sqrt{\tau} = \sqrt{\tau_y} + \sqrt{\mu \dot{\gamma}}$

$$\sqrt{\frac{r}{2} \frac{dp}{dx}} = \sqrt{\tau_y} + \sqrt{\mu \dot{\gamma}} \leftarrow \text{rate of strain: } \dot{\gamma} = \frac{dv}{dr}$$

dynamic viscosity



$$\begin{aligned} u(r) &= \frac{1}{\mu} \int \left(\sqrt{\frac{r}{2} \frac{dp}{dx}} - \sqrt{\tau_y} \right)^2 dr \\ &= \frac{1}{\mu} \int \left(\sqrt{\frac{r}{R_c}} \sqrt{\tau_y} - \sqrt{\tau_y} \right)^2 dr = \frac{\tau_y}{\mu} \int \left(\sqrt{\frac{r}{R_c}} - 1 \right)^2 dr \\ &= \frac{\tau_y}{\mu} \int \frac{r}{R_c} - 2\sqrt{\frac{r}{R_c}} + 1 dr = \frac{\tau_y}{\mu} \left(\frac{r^2}{2R_c} - \frac{4\sqrt{R_c}}{3} r^{3/2} + r + C \right) \end{aligned}$$

$$u(R) = 0 = \frac{\tau_y}{\mu} \left(\frac{R^2}{2R_c} - \frac{4\sqrt{R_c}}{3} R^{3/2} + R + C \right) \Rightarrow C = -\frac{R^2}{2R_c} + \frac{4\sqrt{R_c}}{3} R^{3/2} - R$$

$Q_f: r > R_c$ fluid flow

$Q_p: r \leq R_c$ travel as plug (no flow) } $\oplus Q_{\text{ges}}$

$\checkmark Q_p = \int_0^{R_c} u(r) 2\pi r dr = \frac{1}{\mu} (-3.154 \cdot 10^{-3} \text{ dyn} \cdot \text{cm})$

u plug from S.31 in pdf! & task 1.3

$$\left(Q_f = \int_{R_c}^R u(r) 2\pi r dr = \frac{1}{\mu} (-20.103 \cdot 10^{-3} \text{ dyn} \cdot \text{cm}) \right)$$

$$\Rightarrow \frac{Q_p}{Q_f + Q_p} = 13.56\% \text{ travels as plug}$$

$$Q_{\text{total}} = -\frac{\pi R^4}{8\mu} \frac{dp}{dx} \cdot \frac{R_c}{R} \quad \text{S.32 in pdf}$$

$$\begin{aligned} Q_{\text{plug}} &= \int u_{\text{plug}} dA = \int_0^{R_c} u_{\text{plug}} 2\pi r dr \\ u_{\text{plug}} &= -\frac{1}{4\mu} \frac{dp}{dx} \left[R^2 - \frac{8}{3} \sqrt{R_c} R^{3/2} + 2R_c R - \frac{4}{3} R_c^{3/2} \right] \\ a &= 0.010936 \text{ cm}^2 \\ Q &= \int_0^{R_c} -\frac{1}{4\mu} \frac{dp}{dx} a 2\pi r dr = -\frac{2\pi}{4\mu} \frac{dp}{dx} a \frac{R_c^2}{2} \end{aligned}$$

$$\begin{aligned} Q_{\text{total}} &= -\frac{\pi R^4}{8\mu} \frac{dp}{dx} f(\xi) \quad f(\xi) = 0.1476 \\ Q_{\text{plug}} &= -\frac{2\pi}{4\mu} \frac{dp}{dx} a \frac{R_c^2}{2} \\ \frac{Q_{\text{plug}}}{Q_{\text{total}}} &= \frac{-\frac{2\pi}{4\mu} \frac{dp}{dx} a \frac{R_c^2}{2}}{-\frac{\pi R^4}{8\mu} \frac{dp}{dx}} = \frac{\frac{1}{2} a \frac{R_c^2}{2}}{\frac{1}{8} R^4 f(\xi)} = 0.133 \end{aligned}$$

1.2 Casson fluid – pressure drop

A 40 cm long tube (internal diameter, 1 mm) is filled with blood, which has been citrated to prevent it from clotting. (Assume that citration does not alter the rheological properties of the blood.) Using the property values for blood: $\mu = 3.5 \text{ cP}$, $\tau_y = 0.05 \text{ dynes/cm}^2$, $\rho = 1.06 \text{ g/cm}^3$.

$1 \text{ Pa} = 10 \frac{\text{dyn}}{\text{cm}^2}$

- (a) At what pressure difference between the tube ends (Δp) does the blood begin to flow?
- (b) What is the flow rate (Q) when $\Delta p = 20 \text{ Pa}$? How long would it take for 10ml of blood to flow through the tube?
- (c) In comparison, how long would it take for 10ml water (a Newtonian fluid with $\mu = 1 \text{ cP}$), to travel through the tube with the same pressure difference between the tube ends.

$1 \text{ cP} = 0.001 \text{ Pa} \cdot \text{s}$

a) begins to flow when shear stress equals yield stress
 $\tau_w > \tau_y = \frac{\Delta p R}{2L} \Rightarrow \Delta p = \frac{\tau_w \cdot 2 \cdot L}{\frac{1}{2}} = \frac{5 \cdot 10^{-3} \text{ Pa} \cdot 2 \cdot 0.4 \text{ m}}{0.5 \cdot 10^{-3} \text{ m}} = 8 \text{ Pa}$

b) $R_c = \frac{2 \tau_y L}{\Delta p} = \frac{5 \cdot 10^{-3} \text{ Pa} \cdot 2 \cdot 0.4 \text{ m}}{200 \frac{\text{dyn}}{\text{cm}^2}} = 0.2 \text{ mm}$
 $t = \frac{V}{Q} = \frac{10 \text{ ml} \cdot 1.06}{1000} \cdot \frac{1}{3.036 \cdot 10^{-4}} = 34.46 \text{ s}$

a) $\tau_y = \frac{\Delta p R}{2L} \Rightarrow \Delta p = \frac{\tau_w \cdot 2L}{R} = 8 \text{ Pa}$
 $1 \text{ Pa} \hat{=} 10 \frac{\text{dyn}}{\text{cm}^2}$
b) $Q_{\text{wall}} = -\frac{\pi R^4}{8\mu} \frac{dp}{dx} F(\xi)$
 $R_c = \frac{2 \tau_y L}{\Delta p} = 0.2 \text{ mm}$
 $\xi = \frac{0.2 \text{ mm}}{0.5 \text{ mm}} = 0.4$
 $F(\xi) = 0.0865$
 $\mu = 1 \text{ cP} \hat{=} 0.001 \text{ Pa} \cdot \text{s}$
 $Q = -\frac{\pi R^4}{8\mu} \frac{dp}{dx} F(\xi) = -3.033 \cdot 10^{-5} \text{ cm}^3/\text{s}$
 $V = 10 \text{ cm}^3 \Rightarrow Q = \frac{V}{t} \Rightarrow t = \frac{V}{Q} = 329.711 \text{ s}$
 $\approx 9 \text{ min} \approx 3.82 \text{ days}$
c) $Q = \frac{\pi R^4}{8\mu L} \frac{dp}{dx} F(\xi)$
 $t = \frac{V}{Q} = 8130 \text{ s}$

c) Newtonian fluid: $Q = \frac{\pi R^4 \Delta p}{8 \mu L} = 1.23 \cdot 10^{-9} \frac{\text{L}}{\text{s}}$
 $t = \frac{V}{Q} = \frac{0.01}{1.23 \cdot 10^{-9}} = 8.13 \cdot 10^3 \text{ s}$

$Q = \frac{\pi R^4 \Delta p}{8 \mu L} = \frac{\pi (0.0005 \text{ m})^4 \cdot 20 \text{ Pa}}{8 \cdot 0.001 \text{ Pa} \cdot \text{s} \cdot 0.4 \text{ m}}$
 $t = \frac{10 \cdot 10^{-6} \text{ m}^3 \cdot 1.06}{Q} = 135 \text{ min} = 2.26 \text{ h}$

1.3 Casson fluid – flow between two plates

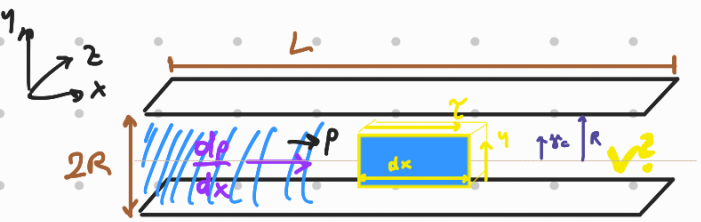
A Casson fluid fills the space between two horizontally positioned, parallel plates. The plates are very large, in comparison to the distance between them. A pressure gradient $\frac{dp}{dx}$ forces the fluid from left to right. Derive an expression for the velocity of the plug flow region in this flow. Specifically show that for plates at a distance $2R$ from each other:

kommt aber zur Prüfung
wrs! nicht!

$$u_{plug} = -\frac{1}{2\mu} \frac{dp}{dx} \left(R^2 - \frac{y_c^2}{3} - \frac{8}{3} \sqrt{y_c R^3} + 2y_c R \right)$$

Where μ is the parameter from the Casson relationship and $R - y_c$ is the distance between the plate and the edge of the plug flow region (or, in other words, y_c is the distance between the center-line between the plates and the edge of the plug flow region)

Hint: The derivation is very similar to the derivation for a cylindrical tube.



no shear stress along y
(compared to cylinder)

$$p \cdot 2y + 2 \tau \, dx = (p + dp) \, 2y \cdot dz$$

$$\Rightarrow \tau = \frac{dp}{dx} \cdot y$$

$$\tau_y = \frac{dp}{dx} \, y_c$$

$$\sqrt{\tau} = \sqrt{\tau_y} + \sqrt{\mu \cdot \dot{\gamma}} \quad \dot{\gamma} = \frac{du}{dy}$$

$$\sqrt{\frac{dp}{dx} y} - \sqrt{\frac{dp}{dx} y_c} = \sqrt{\mu \frac{du}{dy}} \quad | \cdot 2$$

Handwritten derivation of the velocity profile for a Casson fluid in a channel. It shows the force balance, the Casson model equation, and the integration to find the velocity $u(y)$.

boundary conditions: $u(R) = 0$

= mein 1. Bsp...

$$\begin{aligned} u(y) &= \frac{1}{\mu} \frac{dp}{dx} \left(\frac{1}{2} (y^2 - R^2) - \frac{4}{3} \sqrt{y_c} (\sqrt{y^3} - \sqrt{R^3}) + y_c (y - R) \right) \\ &= \frac{1}{2\mu} \left(-\frac{dp}{dx} \right) \left(R^2 - y^2 - \frac{8}{3} \sqrt{y_c} (\sqrt{R^3} - \sqrt{y^3}) + 2y_c (R - y) \right) \\ u(y_c) &= \frac{1}{2\mu} \left(-\frac{dp}{dx} \right) \left(R^2 - y_c^2 - \frac{8}{3} \sqrt{y_c} \sqrt{R^3} + \frac{8}{3} \sqrt{y_c} \sqrt{y_c^3} + 2y_c R - 2y_c^2 \right) \\ &= \frac{1}{2\mu} \left(-\frac{dp}{dx} \right) \left(-\frac{1}{3} y_c^2 + R^2 + 2y_c R - \frac{8}{3} \sqrt{y_c R^3} \right) \end{aligned}$$

2 The heart

Based on the averaged left-ventricular pressure-volume loop (Figure 1), calculate the pumping power of the female and the male heart (left ventricle only). Assume a resting heart rate of 70 beats per minute and approximate the area under the curve with a rectangle.

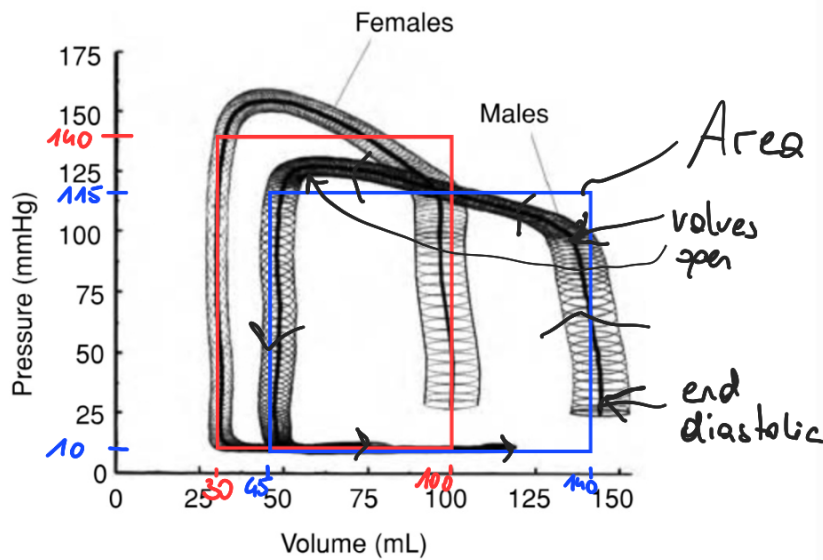


Figure 1: Left ventricular pressure-volume loop

$$f = 70 \text{ bpm} = \frac{70}{60} \frac{1}{s} = 1,16 \text{ Hz}$$

$$1 \text{ mmHg} \hat{=} 133,32 \text{ Pa} = \frac{\text{N}}{\text{m}^2} = \frac{\text{kg}}{\text{m} \cdot \text{s}^2}$$

$$(1 \text{ ml blood} \hat{=} 1,06 \text{ g})$$

$$[W] = \frac{\text{m}^2 \cdot \text{kg}}{\text{s}^3}$$

$$\text{Female: } A_F = \frac{100-50}{10^6} (140-30) \cdot 133,32 = 1,213 \frac{\text{kgm}^2}{\text{s}^2}$$

$$P_F = A_F \cdot f = 1,41 \text{ W}$$

$$\text{Male: } A_n = \frac{140-45}{10^6} \cdot (115-10) \cdot 133,32 = 1,329 \frac{\text{kgm}^2}{\text{s}^2}$$

$$P_n = A_n \cdot f = 1,55 \text{ W}$$

